

Fig. 2. Rate profile for the CRL-catalysed esterification of *rac*-2-methyloctanoic acid with *n*-tetradecanol  $\blacksquare$  : with added  $\text{Na}_2\text{SO}_4 / \text{Na}_2\text{SO}_4 \cdot 10 \text{H}_2\text{O}$  and  $\times$  : without added salts.

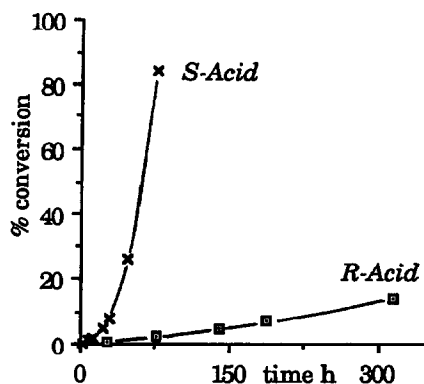


Fig. 3. CRL-catalysed esterification of  $\times$  : (*S*)- (87.3 % *ee*) and  $\blacksquare$  : (*R*)-2-methyloctanoic acid (97.4 % *ee*) with *n*-dodecanol in cyclohexane without added salts.

We now wish to report our results obtained from the esterification of 2-methyloctanoic acid with an excess of *n*-do- and *n*-tetradecanols, respectively, using the same batch of stored CRL as the catalyst in cyclohexane at 25° without or with either added anhydrous sodium hydrogen phosphate / sodium hydrogen phosphate dihydrate or anhydrous sodium sulphate / sodium sulphate decahydrate mixture. These salt mixtures are known to maintain water activities of  $a_w = 0.15$  and 0.76 respectively.<sup>7</sup>

The resolutions were performed as follows: the acid (3.75 mmol) and the alcohol (22.5 mmol) and an internal standard were dissolved in cyclohexane (25 ml). In some experiments salt mixtures of either  $\text{Na}_2\text{HPO}_4 / \text{Na}_2\text{HPO}_4 \cdot 2\text{H}_2\text{O}$  (equimolar amounts, 1.3 g) or  $\text{Na}_2\text{SO}_4 / \text{Na}_2\text{SO}_4 \cdot 10\text{H}_2\text{O}$  (equimolar amounts, 1.8 g) was present. After stirring (10 min) the crude enzyme powder (Sigma, stored as mentioned above, 1.69 g, corresponding to  $1.5 \times 10^6$  units) was added. The mixture was stirred in a closed flask at ambient temperature and samples were withdrawn at intervals. Conversions were determined by gas chromatography. The enantiomeric excesses of the esters produced were determined by reduction ( $\text{LiAlH}_4$ ) to the 2-methyl-1-alkanol followed by oxidation to the acid and conversion to the amide with (*S*)-1-phenylethylamine and GC-analyses of the diastereomeric mixtures on a Carbowax-type column.<sup>2b</sup> Contrary to direct alkaline hydrolysis - acidification of the esters, the reduction - oxidation protocol does not lead to any detectable racemization of the resultant acid.<sup>2b</sup>

The esterification reaction of racemic 2-methyloctanoic acid and *n*-tetradecanol catalysed by a stored sample of CRL without added salt shows a rate profile (see Fig. 2.) with an induction period before the reaction rate increases. The apparent *E*-values<sup>8</sup> measured in two separate experiments from *ee* of the product esters were  $23 \pm 2$  at < 35 % conversion. However, if the salt mixture of sodium sulphates was present, the rate profile is much more linear up to close to 40 % conversion (see Fig. 2.). In this case the *E*-values determined at < 35 % conversion were  $91 \pm 10$  in two separate experiments.

The ratios between the initial rates for the pure enantiomers determined separately may in some cases differ from the *E*-values determined from the racemate using the same conditions.<sup>9</sup> However, below we have used these ratios as rough approximations of the *E*-values and assumed a linear relationship between these and the enantiomeric composition of the substrate.

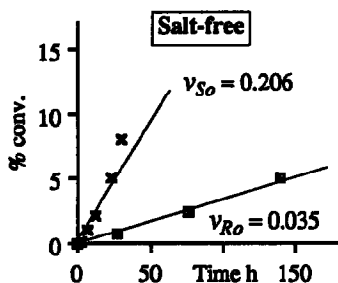


Fig. 4 Initial stages of CRL-catalysed esterifications of **x** : (S)- (87.3 % ee) and **a** : (R)-2-methyloctanoic acid (97.4 % ee) with *n*-dodecanol in cyclohexane without added salts.

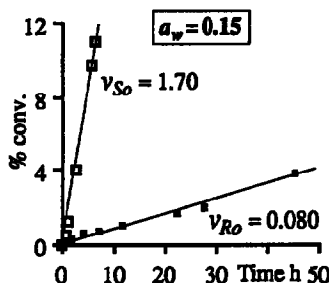


Fig. 5 Initial stages of CRL-catalysed esterifications of **c** : (S)- (87.3 % ee) and **m** : (R)-2-methyloctanoic acid (99.8 % ee) with *n*-dodecanol in cyclohexane with added  $\text{Na}_2\text{HPO}_4/\text{Na}_2\text{HPO}_4 \cdot 2\text{H}_2\text{O}$ .

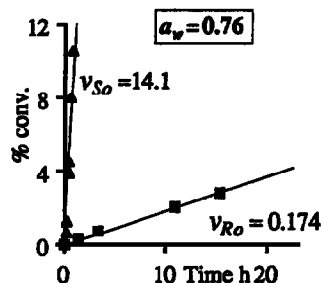


Fig. 6 Initial stages of CRL-catalysed esterifications of **A** : (S)- (73.1 % ee) and **B** : (R)-2-methyloctanoic acid (99.8 % ee) with *n*-dodecanol in cyclohexane with added  $\text{Na}_2\text{SO}_4/\text{Na}_2\text{SO}_4 \cdot 10\text{H}_2\text{O}$ .

Using stored enzyme and salt-free conditions, the individual enantiomers of 2-methyloctanoic acid were esterified with *n*-dodecanol and the rate profiles obtained are described in Figs. 3 and 4. At conversions below 6 %, straight lines were observed which enabled calculation of the initial rates  $v_{S0}$  and  $v_{R0}$  (% conversion / h). From  $v_{S0}$  and  $v_{R0}$  the estimated rates  $v_{S0}^{100}$  and  $v_{R0}^{100}$  for (S)- or (R)-2-methyloctanoic acid of 100 % ee respectively can be calculated assuming that  $v_0 = v_{S0}^{100} \cdot (1-x) + v_{R0}^{100} \cdot x$ , where  $x$  represents the initial proportion of the R-acid. The enantiomeric ratio at the starting point,  $E_0$  was then roughly approximated by the initial rate ratio  $v_{S0}^{100} / v_{R0}^{100} = 7 = E_0$ . As seen in Fig. 3, not only do the rates for both enantiomers above 6 - 10 % conversion increase, but also the rate ratio  $v_S / v_R$ ; i. e. the *E*-value increases as the salt-free reactions proceed, probably due to increased  $a_w$  since water is produced in the esterification. When esterifying racemic acid using salt-free conditions and fresh enzyme, an apparent  $E = 40$  at  $\approx 40$  % conv. (from ee of the product<sup>8</sup>) is registered, which should be the integrated result of a lower *E* at the start compensated by a higher *E* at 40 % conversion.

In contrast to the salt-free case, experiments with the same stored enzyme batch performed under identical conditions except for the presence of salt mixtures gave linear plots over wide conversion ranges (for *S*-acids up to at least 50 %; the reactions with *R*-acids were linear at least up to the point of interruption = 10 %). Thus the phosphate salt mixture of low water activity ( $a_w = 0.15$ ; Fig. 5.) led to  $v_{S0}^{100} / v_{R0}^{100} = 23 = E_0$  whereas the sulphate salt mixture of high water activity ( $a_w = 0.76$ ; Fig. 6.) resulted in a  $v_{S0}^{100} / v_{R0}^{100} = 95 = E_0$ . (both  $E_0$ -values calculated as described above). A similar *E*-value ( $83 \pm 10$ ) was determined<sup>2b</sup> for the esterification of dodecanol and *rac*-2-methyloctanoic acid by end point determination from ee of the product<sup>8</sup> at  $\approx 30$  % conversion using freshly delivered enzyme, without prior storage.

Even if the true *E*-values for esterification of the racemic acid should differ from the initial rate ratios between the individual enantiomers measured under otherwise identical conditions, we expect the dependance on water activity to be very similar for the rate ratios and the *E*-values. Thus, we have demonstrated that, at least for the CRL-enzyme system studied here it is very important to control the water activity not only, as earlier noted, for obtaining high reaction rates but also for maximum enantioselectivity. Further studies are under way.

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**References and notes**

1. For some recent reviews: (a) Engel, K. H. *ACS symposium series* **1992**, *490*, 21-31. (b) Hult, K.; Norin, T. *Pure Appl. Chem.* **1992**, *64*, 1129-1134.
2. (a) Holmberg, E.; Holmquist, M.; Hedenström, E.; Berglund, P.; Norin, T.; Högberg, H.-E.; Hult, K. *Appl. Microbiol. Biotechnol.* **1991**, *35*, 572-578. (b) Berglund, P.; Holmquist, M.; Hedenström, E.; Hult, K.; Högberg, H.-E. *Tetrahedron: Asymmetry* **1993**, *4*, 1869-1878.
3. (a) Zaks, A.; Klivanov, A. M. *J. Biol. Chem.* **1988**, *263*, 8017-8021. (b) Reslow, M.; Adlercreutz, P.; Mattiasson, B. *Eur. J. Biochem.* **1988**, *177*, 313-318. (c) Bodnár, J.; Gubicza, L.; Szabó, L.-P. *J. Mol. Catal.* **1990**, *61*, 353-361. (d) Goldberg, M.; Thomas, D.; Legoy, M.-D. *Eur. J. Biochem.* **1990**, *190*, 603-609. (e) Goldberg, M.; Thomas, D.; Legoy, M.-D. *Enzyme Microb. Technol.* **1990**, *12*, 976-981. (f) Monot, F.; Borzeix, F.; Bardin, M.; Vandecasteele, J.-P. *Appl. Microbiol. Biotechnol.* **1991**, *35*, 759-765. (g) Kise, H.; Tomiuchi, Y. *Biotechnol. Lett.* **1991**, *13*, 317-322. (h) van Erp, S. H. M.; Kamenskaya, E. O.; Khmel'nitsky, Y. L. *Eur. J. Biochem.* **1991**, *202*, 379-384. (i) Blanco, R. M.; Rakels, J. L. L.; Guisán, J. M.; Halling, P. J. *Biochim. Biophys. Acta* **1992**, *1156*, 67-70. (j) Sarazin, C.; Goethals, G.; Seguin, J. P.; Legoy, M.-D.; Barbotin, J. N. *Ann. N. Y. Acad. Sci.* **1992**, *672*, 305-313.
4. (a) Goderis, H. L.; Ampe, G.; Feyten, M. P.; Fouwé, B. L.; Guffens, W. M.; Van Cauwenberg, S. M.; Tobback, P. *Biotechnol. Bioeng.* **1987**, *30*, 258-266. (b) Halling, P. J. *Biochim. Biophys. Acta* **1990**, *1040*, 225-228. (c) Adlercreutz, P. *Eur. J. Biochem.* **1991**, *199*, 609-614. (d) Valivety, R. H.; Halling, P. J.; Macrae, A. R. *Indian J. Chem.* **1992**, *31B*, 914-916. (e) Gubicza, L. in *Biocatalysis in Non-Conventional Media*; Tramper, J.; Vermue, M. H.; Beftink, H. H.; von Stockar, U. Eds.; Elsevier Science Publishers, the Netherlands, 1992; pp. 497-503. (f) Valivety, R. H.; Halling, P. J.; Macrae, A. R. in *Biocatalysis in Non-Conventional Media*; Tramper, J.; Vermue, M. H.; Beftink, H. H.; von Stockar, U. Eds.; Elsevier Science Publishers, the Netherlands, 1992; pp. 549-555. (g) Svensson, I.; Adlercreutz, P.; Mattiasson, B. *J. Am. Oil Chem. Soc.* **1992**, *69*, 986-991.
5. (a) Kuhl, P.; Halling, P. J. *Biochim. Biophys. Acta* **1991**, *1078*, 326-328. (b) Kvittingen, L.; Sjursnes, B.; Anthonsen, T.; Halling, P. *Tetrahedron* **1992**, *48*, 2793-2802.
6. (a) Stokes, T. M.; Oehlschlager, A. C. *Tetrahedron Lett.* **1987**, *28*, 2091-2094. (b) Holmberg, E.; Hult, K. *Biocatalysis* **1990**, *3*, 243-251. (c) Kitaguchi, H.; Itoh, I.; Ono, M. *Chem. Lett.* **1990**, 1203-1206. (d) van der Lugt, J. P.; Elfrink, H.; Evenaar, J.; Doddema, H. J. in *Microbial Reagents in Organic Synthesis*; Servi, S. Ed.; Kluwer Academic Publishers, the Netherlands, 1992; pp. 261-272. (e) Wickli, A.; Schmidt, E.; Bourne, J. R. in *Biocatalysis in Non-Conventional Media*; Tramper, J.; Vermue, M. H.; Beftink, H. H.; von Stockar, U. Eds.; Elsevier Science Publishers, the Netherlands, 1992; pp. 577-584. (f) Bovara, R.; Carrea, G.; Ottolina, G.; Riva, S. *Biotechnol. Lett.* **1993**, *15*, 169-174. (g) Bomscheuer, U.; Herar, A.; Kreye, L.; Wendel, V.; Capewell, A.; Meyer, H. H.; Scheper, T.; Kolisis, F. N. *Tetrahedron: Asymmetry* **1993**, *4*, 1007-1016. (h) Högberg, H.-E.; Hedenström, E.; Nordin, O. *To be published*.
7. Halling, P. J. *Biotechnol. Techniques* **1992**, *6*, 271-276.
8. Chen, C.-S.; Fujimoto, Y.; Girdaukas, G.; Sih, C. J. *J. Am. Chem. Soc.* **1982**, *104*, 7294-7299.
9. For a discussion of the use of initial rate ratios for *E* determinations, see: Jongejan, J. A.; van Tol, J. B. A.; Geertlof, A.; Duine, J. A. *Recl. Trav. Chim. Pays-Bas* **1991**, *110*, 247-254.